

TECHNICAL SOLUTIONS TOWARDS AN INTEGRATED OPTIMIZATION OF ENERGY – FIBER FRACTIONATION

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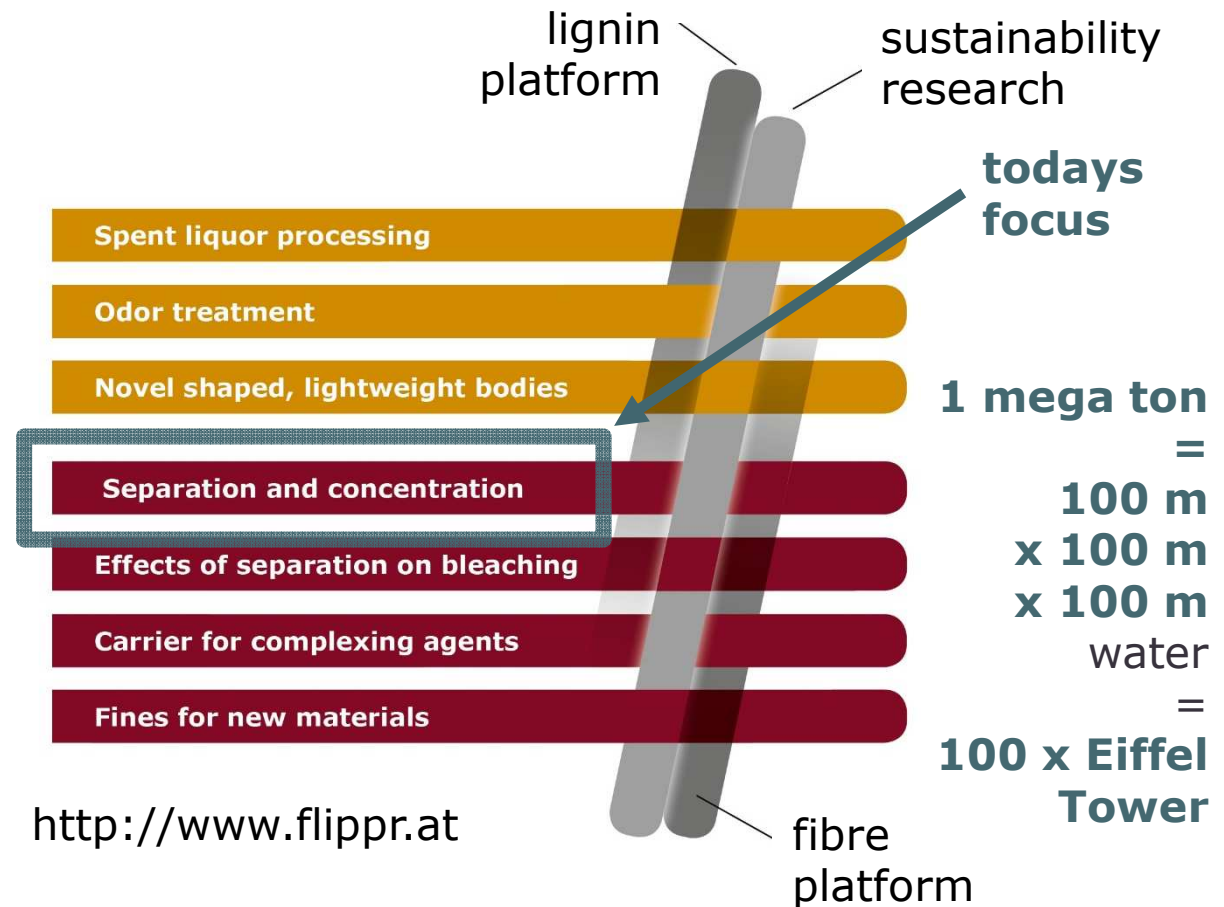
INTRODUCTION

A "Pulp and Paper" biorefinery for us means

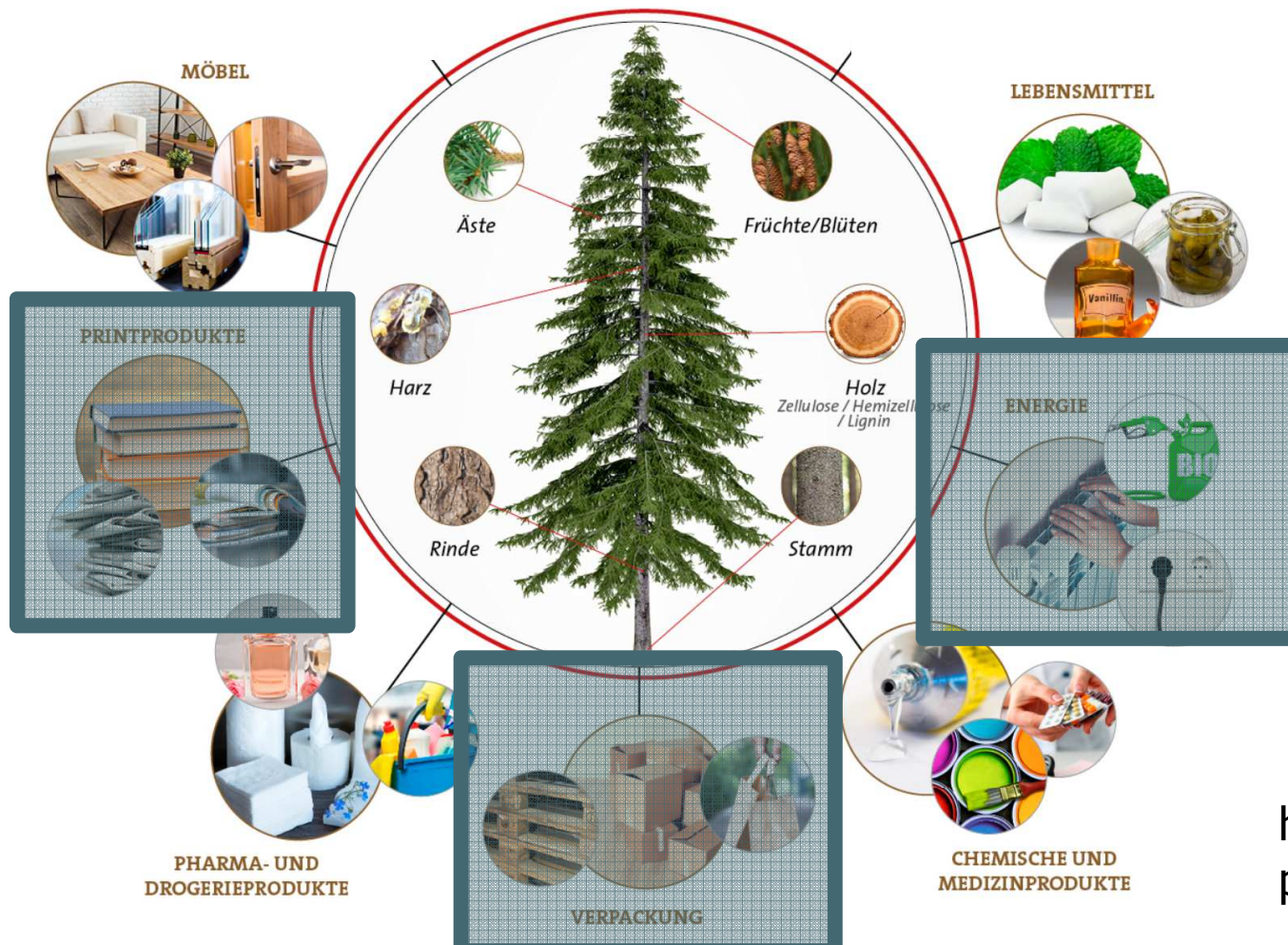
- 1) **Extract & utilize lignin** from classical & existing cooking processes
- 2) **Fractionate** cellulose pulp into **finer and fibres**

Our Mission

...more **added value from wood** on a **mega ton per year** scale



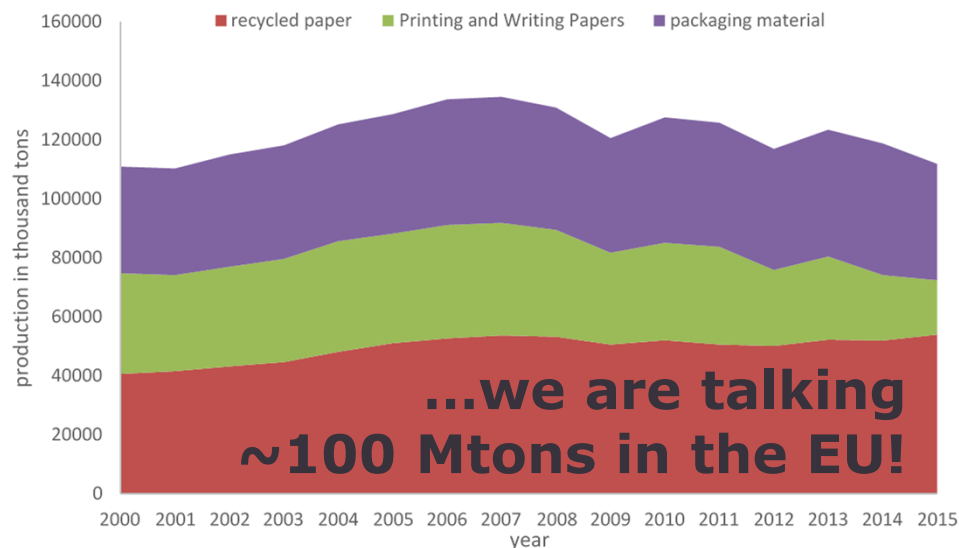
INTRODUCTION



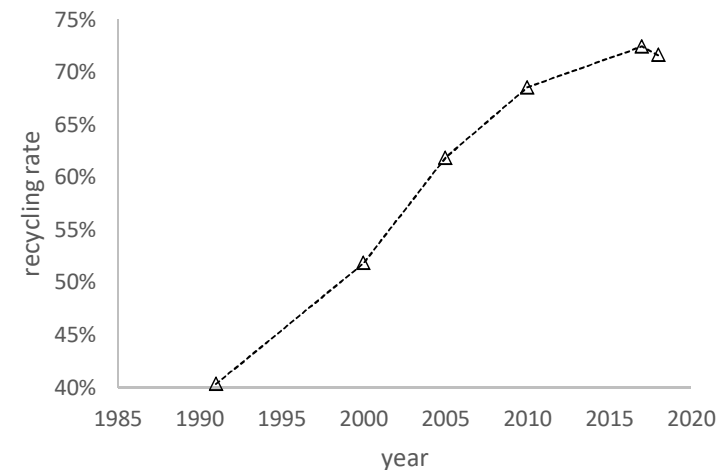
<https://www.austropapier.at>

MOTIVATION

- **Why fibre fractionation?**



EUROSTAT, Faser-und Zellstoffe, Papier und Karton (2018).

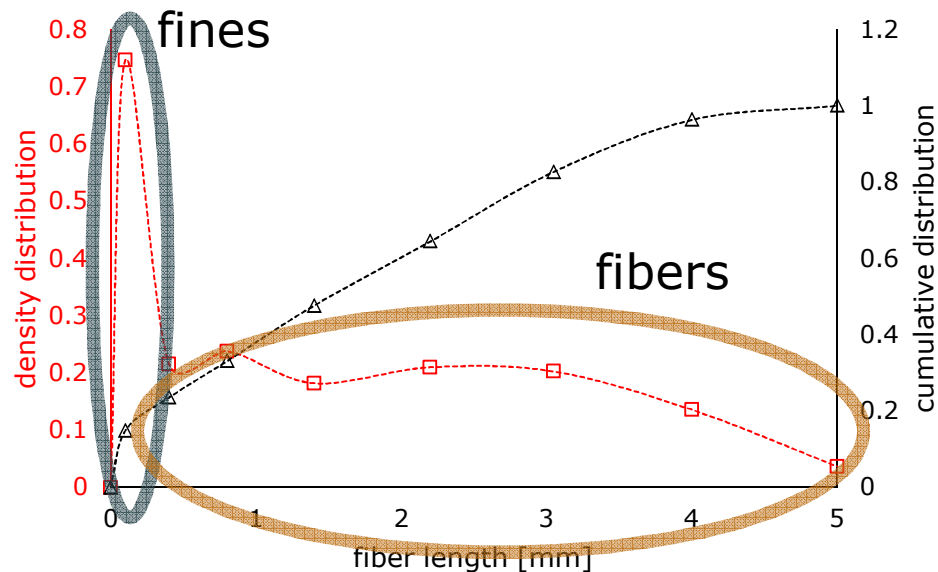


Key statistics European pulp & paper industry, CEPI (2018)

...increasing resource efficiency by a small percentage helps a lot!

MOTIVATION

Fiber length distribution of pulp



Fines

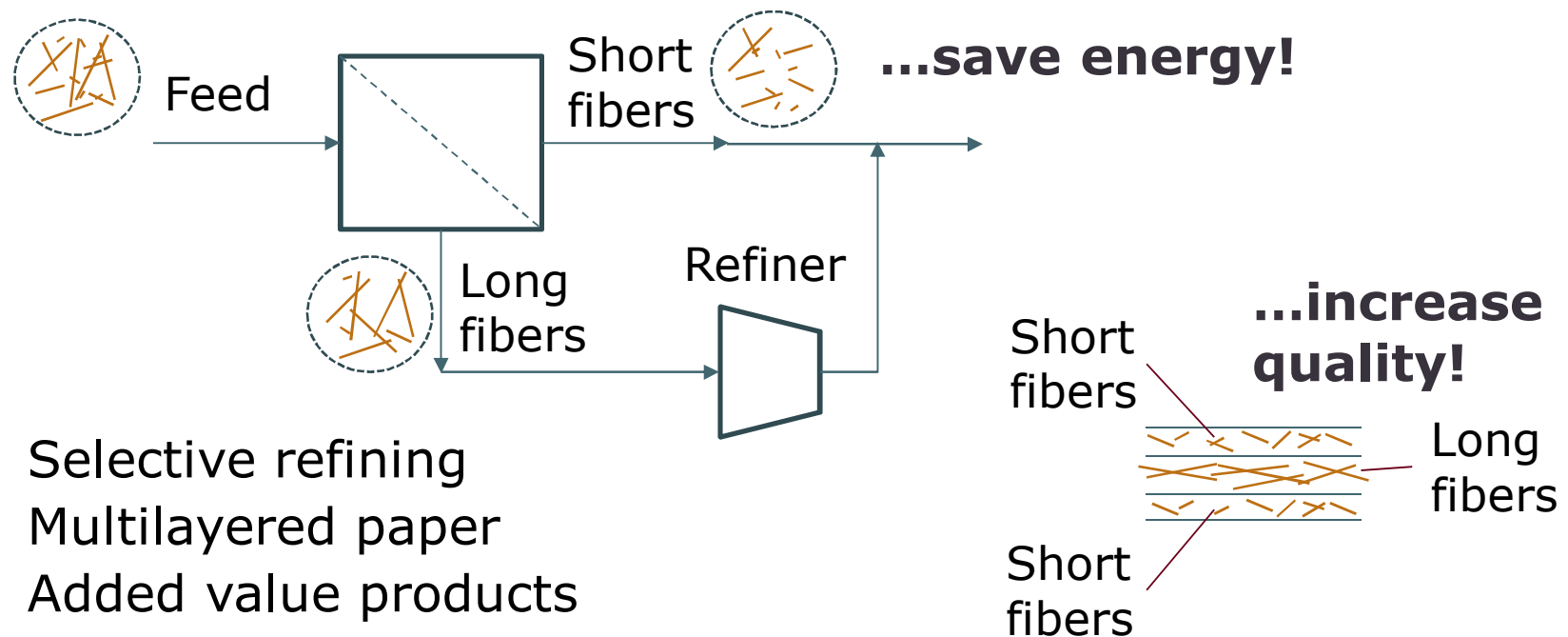
- Increase paper density
- Slow down dewatering
- Consume bleaching chemicals
- Low mass content VS high surface content

Fibers

- Long fibers increase paper strength
- Must be flexibilised (refining)

MOTIVATION

State of the art fractionation concepts

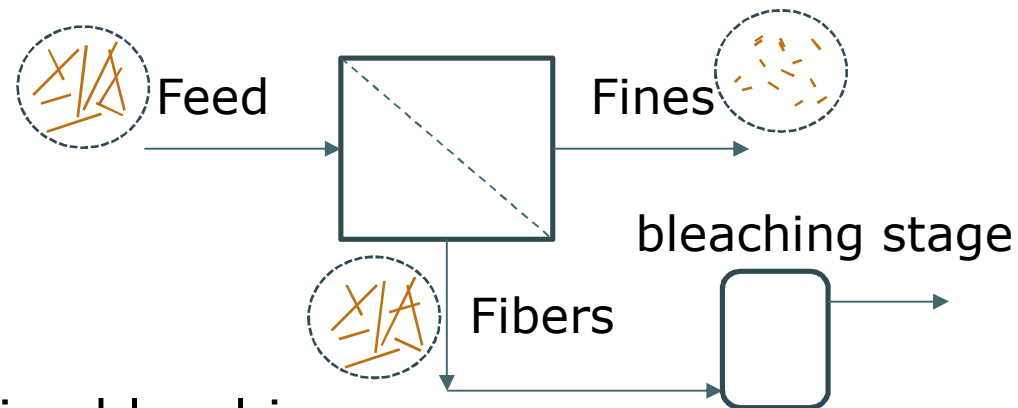


- Selective refining
- Multilayered paper
- Added value products

MOTIVATION

Advanced fractionation concepts

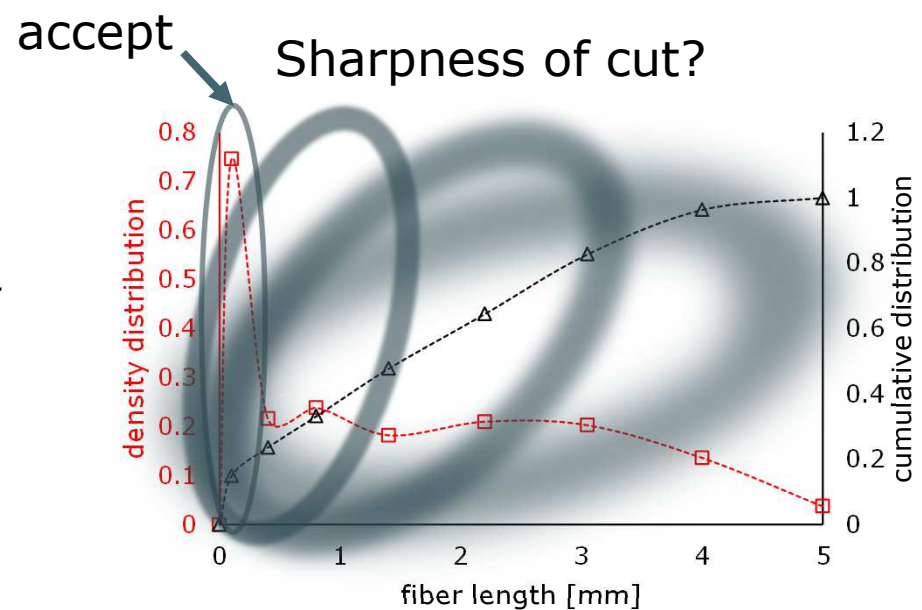
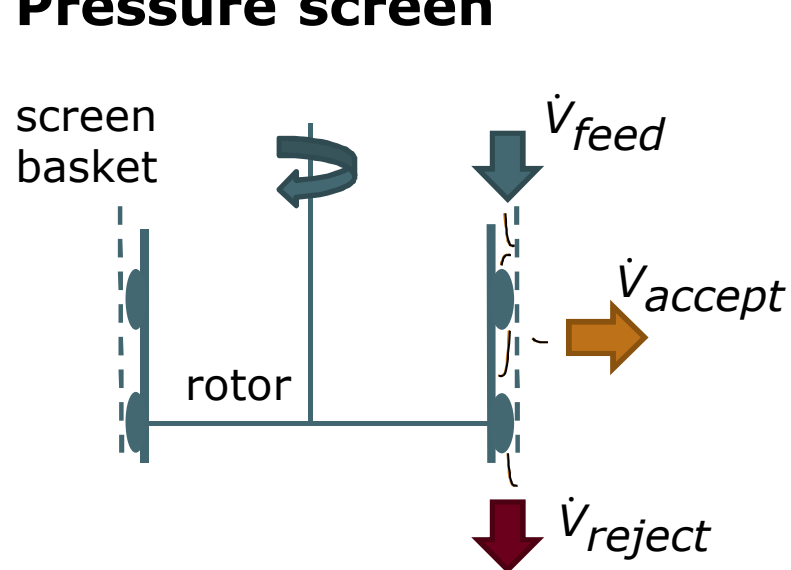
...save resources!



- Selective bleaching
- Fines for new products – “paper VS plastic”
- Process flexibility and control (e.g., for recycled pulp)

FRACTIONATION TECHNOLOGY

Pressure screen

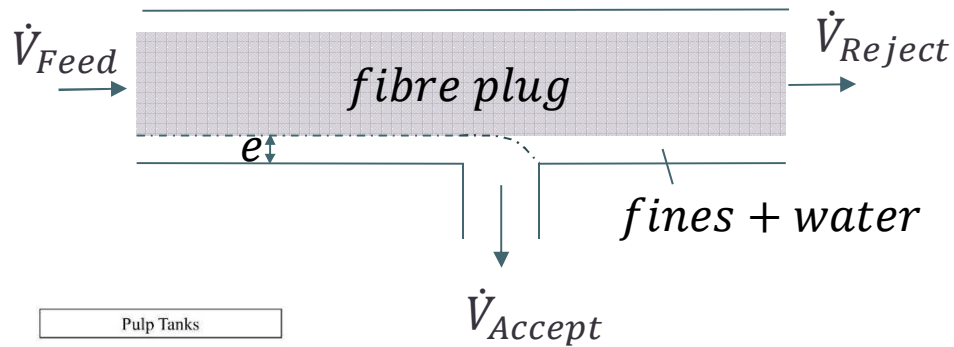


- **high** energy consumption for high selectivity - $P \sim u_{tip}^3$

Delfel et al., Appita 64(1), 2011

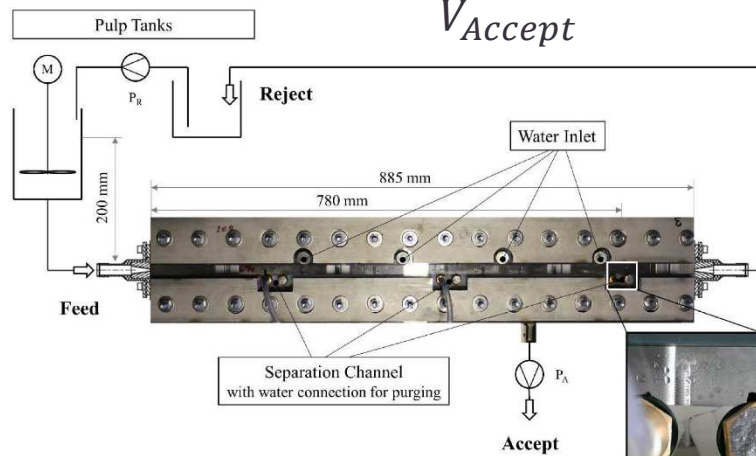
FRACTIONATION TECHNOLOGY

Hydrodynamic Fractionation - The Concept

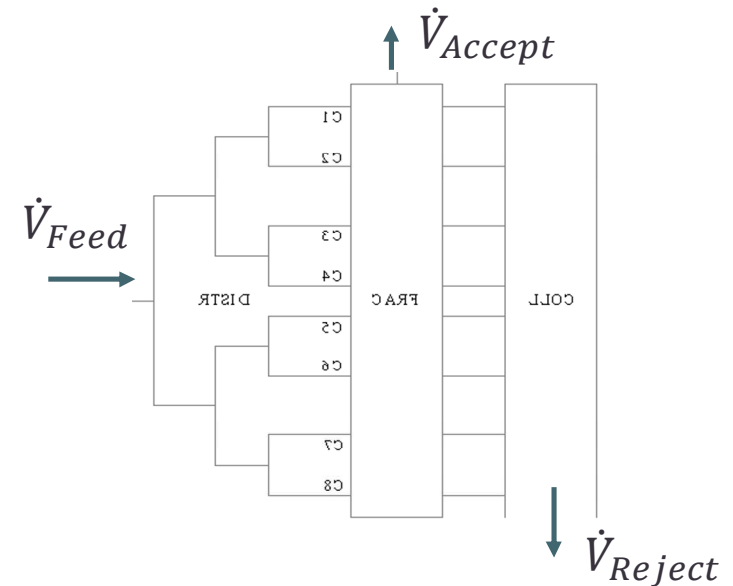


Scale-up strategy

- Numbering-up of channels
- Multi-step design



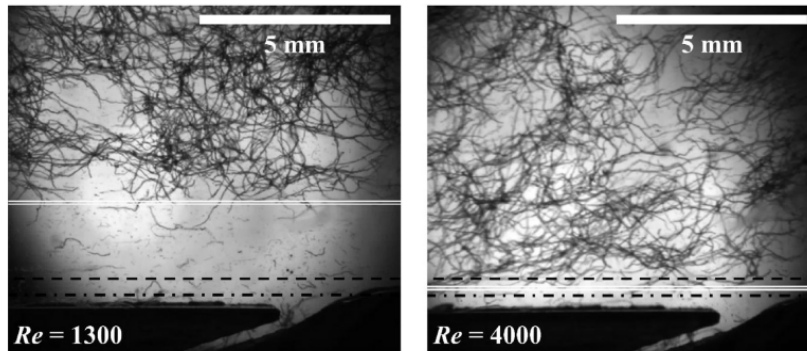
Redlinger-Pohn et al.,
ChERD 126
(2017), 54–66



FRACTIONATION TECHNOLOGY

Hydrodynamic Fractionation

Redlinger-Pohn et al.,
ChERD 126 (2017), 54–66



$Re \approx 1,500 \rightarrow C_{\max} \approx 0.1 [\%]$
high selectivity, but thirsty!

$Re \approx 4,000 \rightarrow C_{\max} \approx 0.5 [\%]$
low selectivity and thirsty!

$Re \approx 1,500 \rightarrow C_{\max} \approx 0.1 [\%]$

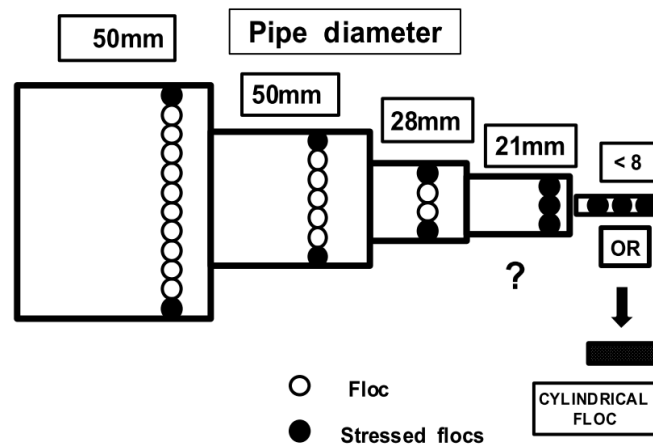
- Number of channels \uparrow
- Apparatus Size \uparrow
- High production cost

$C_{\max} \approx 0.1 [\%]$
↓
• Dilution / Thickening

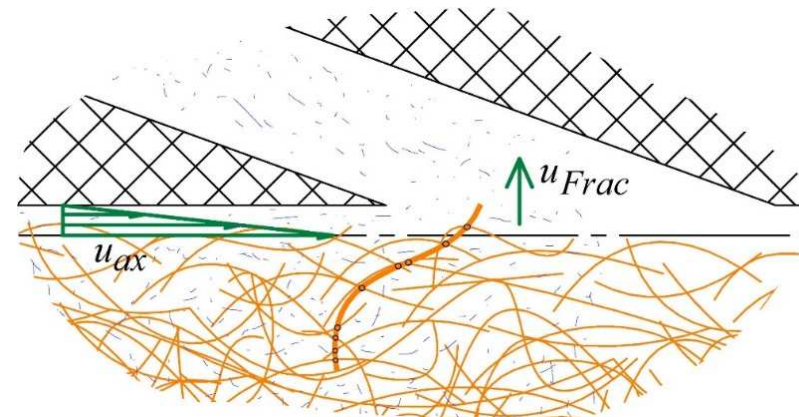
- **High water demand (extremely thirsty!)**

FRACTIONATION TECHNOLOGY

Hydrodynamic Fractionation in a mini-channel - *miniFRAC*



- High selectivity for a wide operational window ($C_{max} > 1.0\%$)



G.G. Duffy, L. Abdullah, Appita J. 56 (2003)

- Compressed, extruded floc
- Stable lubrication layer
- enables fractionation at higher flow speed

FRACTIONATION TECHNOLOGY

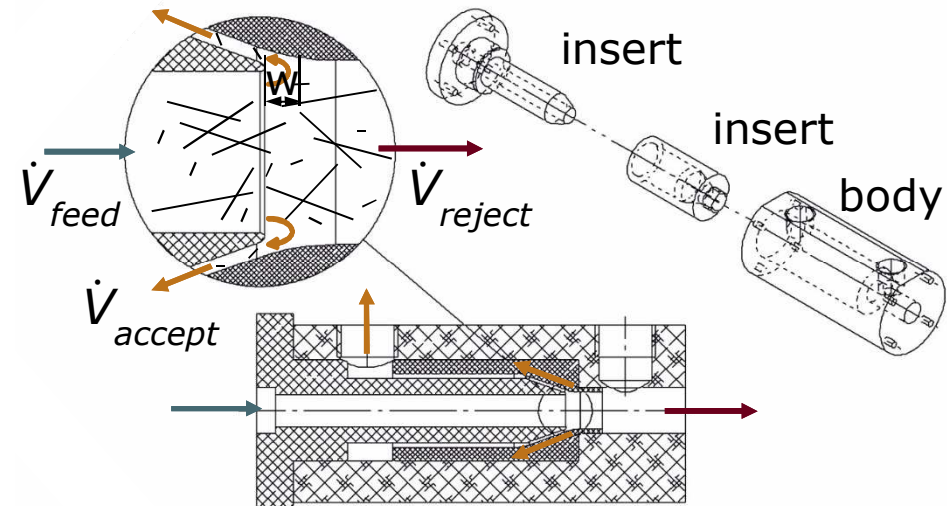
miniFRAC – water-energy nexus

Schmid et al., Nord. Pulp Pap. Res. J. 34(2), 2019

- **no** rotating parts!
- **extremely low** energy consumption

$$P = \dot{V}_{feed} \Delta p;$$
- $\Delta p \approx \Delta p_{water}$

- ✓ **Highly energy efficient**
 - ✓ **Highly water efficient**
- } +



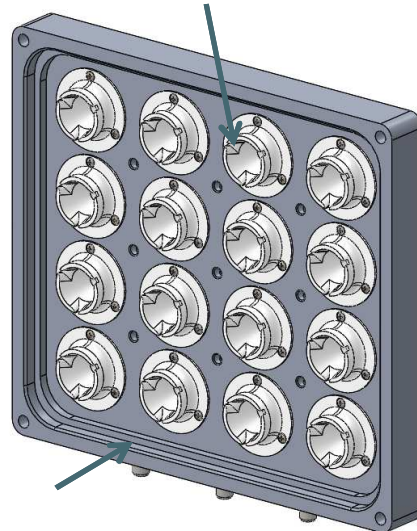
FRACTIONATION TECHNOLOGY

miniFRAC – from lab to industry

...demonstrated on pilot scale at typical industrial consistencies (>2%).

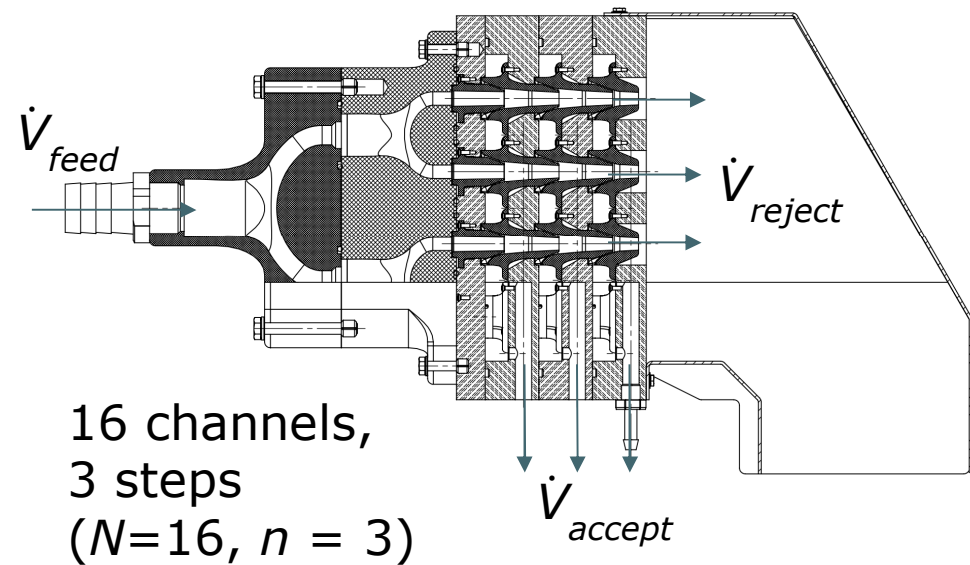
Insert
3D-printed: ABS
Injection molded: PP

Numbering-up of channels



Body
Machined: PP,
aluminum, etc.

Patent AT 521055 B1 2019-10-15



16 channels,
3 steps
($N=16, n=3$)

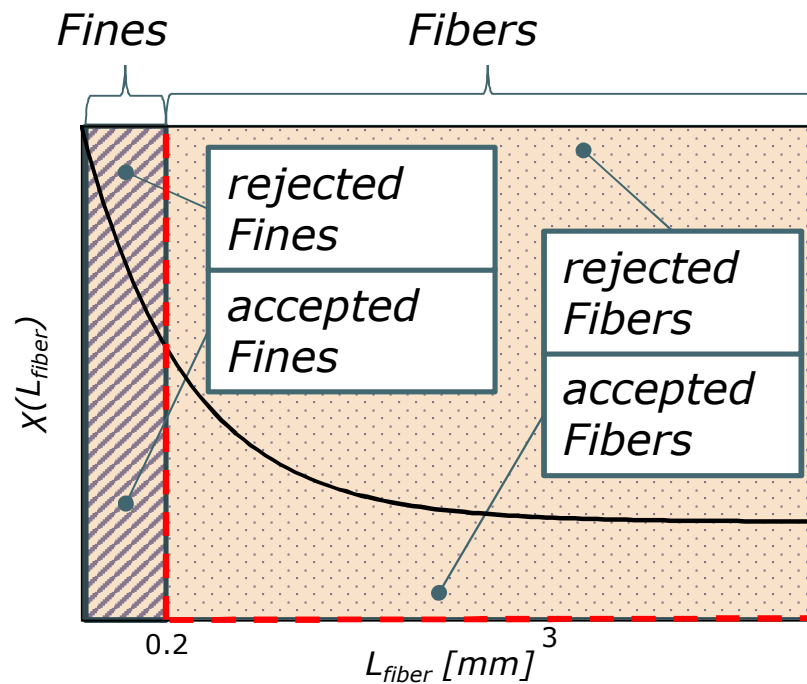
OPERATIONAL WINDOW

Fractionation efficiency

$$\chi(L_{fiber}) = \frac{\dot{m}_{Accept}(L_{fiber})}{\dot{m}_{Feed}(L_{fiber})}$$

$$0 < \chi(L_{fiber}) < 1$$

⇒ relative mass of accepted fibers

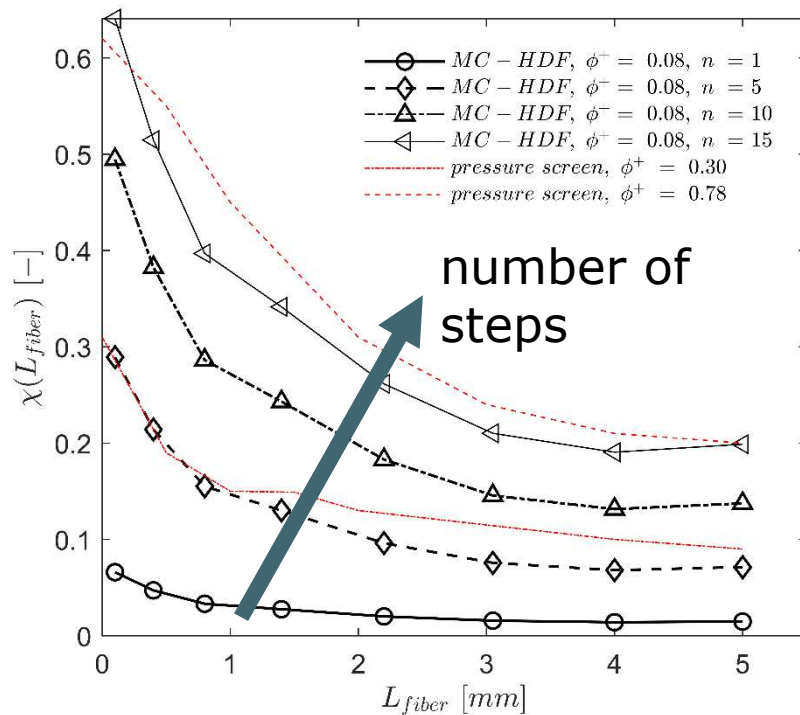


Ideal separation (step function)

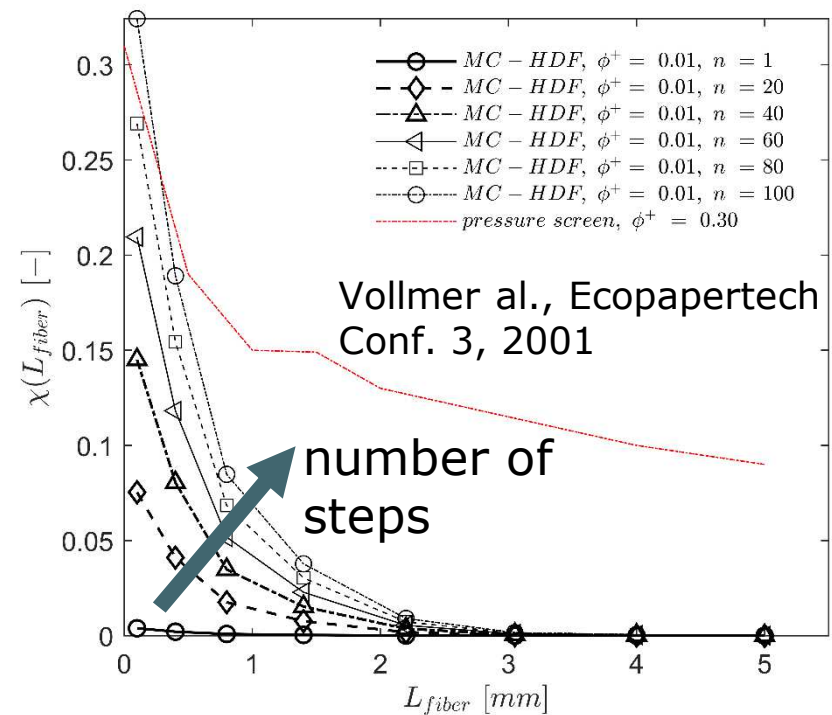
$$\dot{m}_{Accept} = \dot{m}_{fines}$$

OPERATIONAL WINDOW

State of the art fractionation



Highly selective fines fractionation



CONCLUSION 1/2

- ✓ miniFRAC closes gap between
 - “Energy efficiency dilemma” (pressure screen) and
 - “Water efficiency dilemma” (classical hydrodynamic fractionation)

- ✓ New possibilities for pulp & paper industry
 - Selective refining
 - Selective bleaching
 - Multilayered paper
 - Novel fiber based products
 - ... many more

- Adaption to further industries/applications (e.g., carbon fibre recycling)?



source: pixabay.com

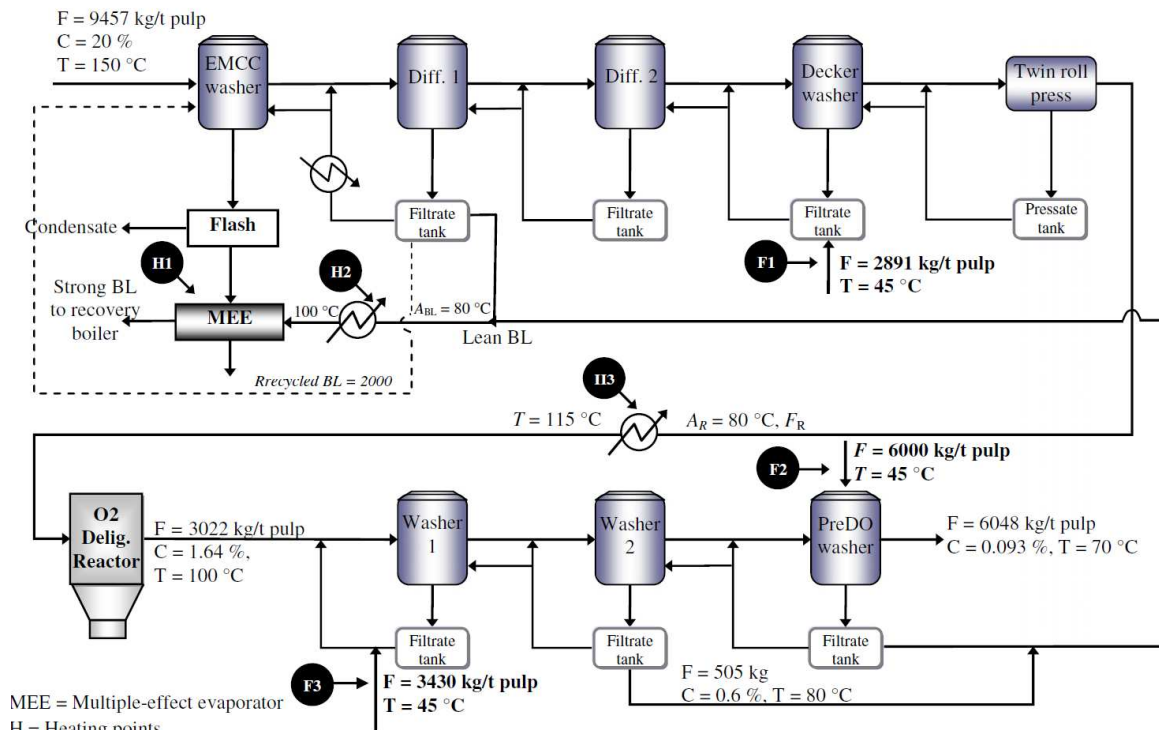
WHERE COULD WE GO NEXT?

- ❑ Realistic Scenario: Kraft Pulp Mill Energy & Water **Optimization**
 - Optimization needs a **mathematical model**
 - Optimization typically goes to „the borders“ of a model. We need a **rigorous model!**
 - **Each process step needs** to be modeled as accurate and rigorous as possible

- ❑ The Challenge: consider a **non-isothermal water-fibres-fines-chemicals** networks
 - Example: **brown stock washing system** (similar to Chew et al., Appl. Thermal Engineering 2013)

WHERE COULD WE GO NEXT?

- Previous work: consider an **isothermal water-fibre-chemicals** network

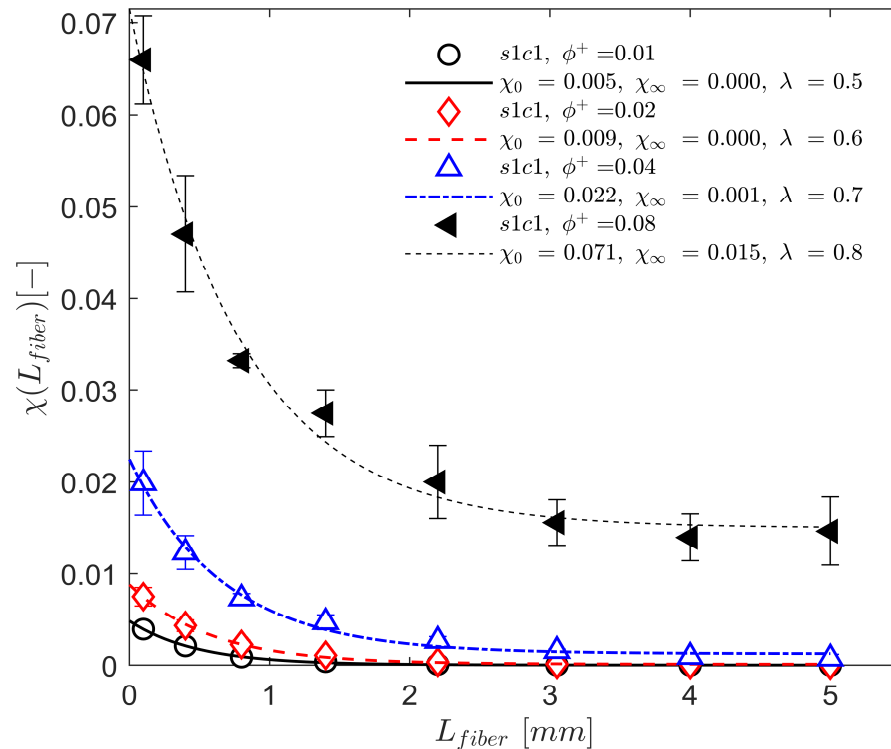


MEE = Multiple-effect evaporator
 H = Heating points
 F = Fresh water points

Chew et al.
 (Appl. Thermal
 Engineering 51
 (2013) 393-400)

WHERE COULD WE GO NEXT?

- Inclusion of fibre-fines separation aspect: predict **fractionation performance** at different operating points



Symbols
Experimental Data

Lines
Model predictions
(inspired by König,
Master Thesis, TU
Graz 2016)

CONCLUSION 2/2

- ✓ Modeling of fibre-fines fractionation process is limiting scientific progress
 - More difficult due to complexity of phenomena
 - Currently purely driven by experiments
 - Quality attributes of product (e.g., fibres) must be defined

- ✓ Optimization framework is already available
 - Non-isothermal water network synthesis & optimization is state of the art in other applications (Ahmetovic et al., CACE 82 (2015) 144–171)

- ✓ Due to modular design of fibre fractionator: optimization on a device-level is also interesting

PROJECT PARTNERS

Industrial partners:



Scientific partners:



FUNDED BY

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