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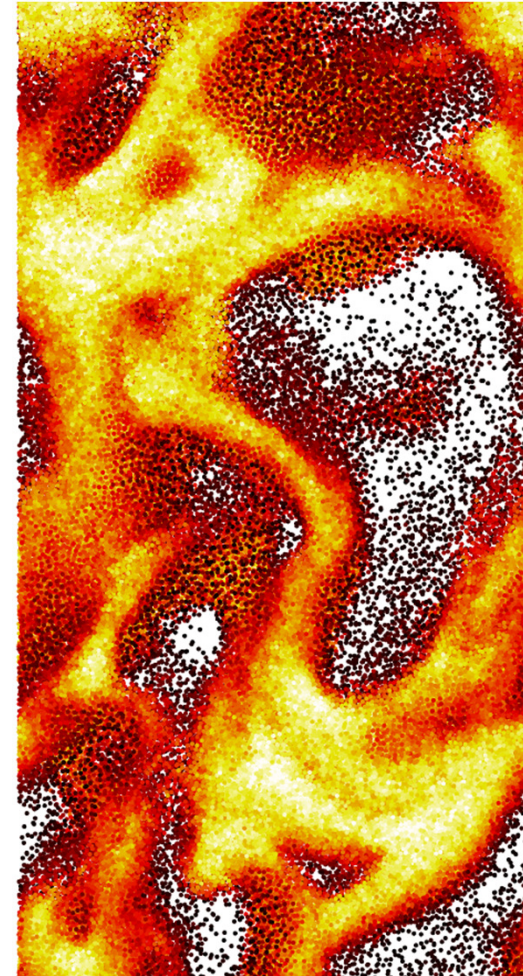
Coarse-Grid Simulations Using Parcels  
**An Advanced Drag Model  
based on Filtered  
CFD-DEM Data**

Stefan Radl and  
Sankaran Sundaresan

Talk 5-4

Fluidization XIV

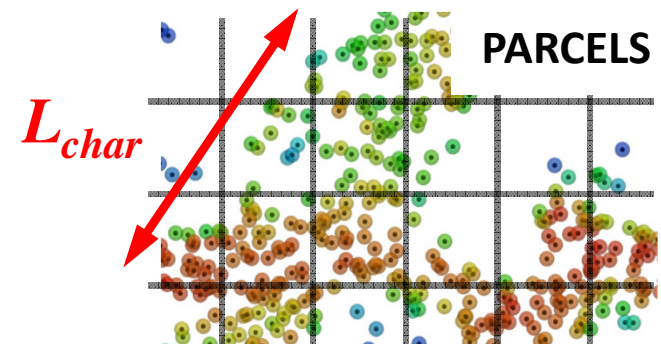
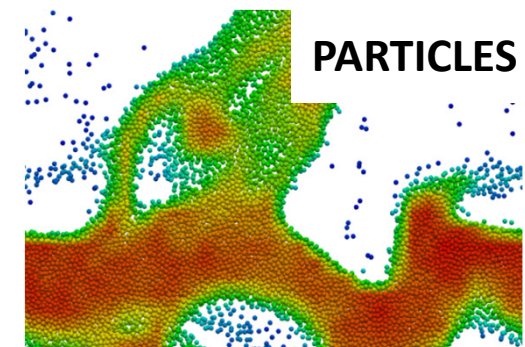
Noordwijkerhout, The Netherlands



# Outline

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- Motivation
- Simulation Setup
- Drag Model Results
- A Short Review of Important Length Scales



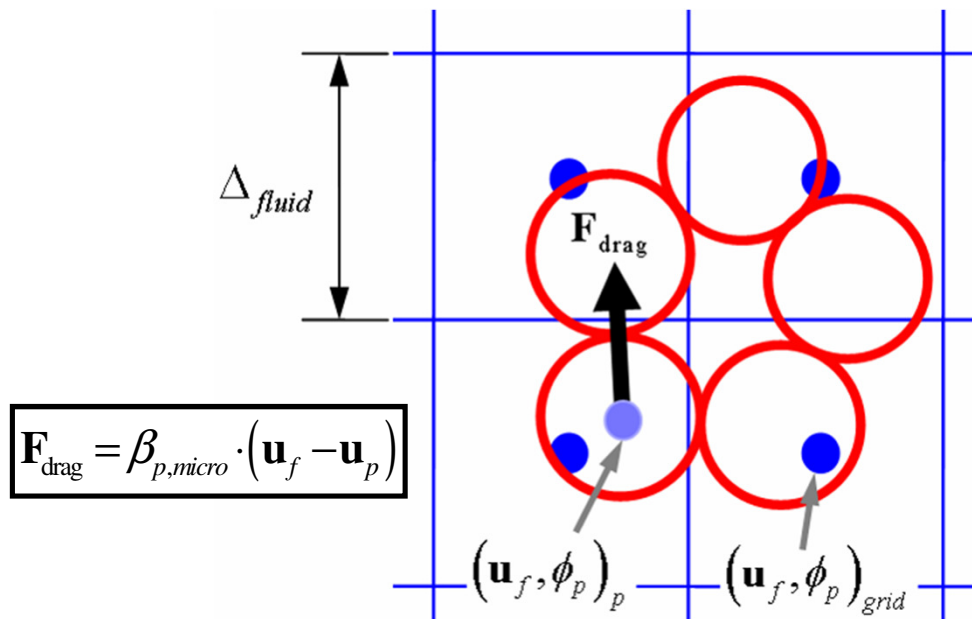
<sup>1</sup>Courtesy: Franklin Shaffer, NETL, Morgantown, WV (2009).

# Simulation Setup

- In the CFD-DEM<sup>2,3</sup> the fluid flow is calculated on a **computational grid that is larger than the particles** - „microscopic“ drag law.
- In the CFD-DPM one computes **virtual „contact“ forces** via a DEM-like tracking of **parcel collisions**.<sup>4</sup> **Microscopic drag law often not suitable.**

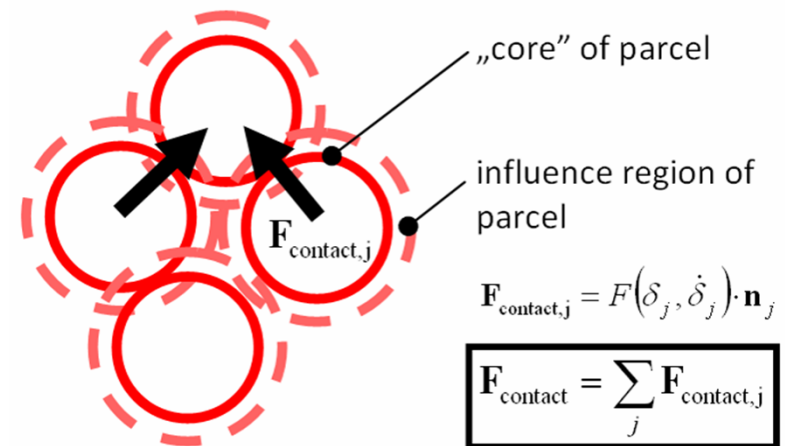
## CFD-DEM

(Zhou et al.,<sup>2</sup> Link et al.<sup>3</sup>)



## (CFD-)DPM

(Patankar and Joseph<sup>4</sup>)



<sup>2</sup>Zhou et al., *JFM* 661 (2010) , <sup>3</sup>Link et al., *Powder Tech* 189 (2009), <sup>4</sup>Patankar and Joseph, *IJMF* 27 (2001).

# Simulation Setup

$$\nabla p = \nabla p_{dyn} + \rho_{mix} \mathbf{g}$$

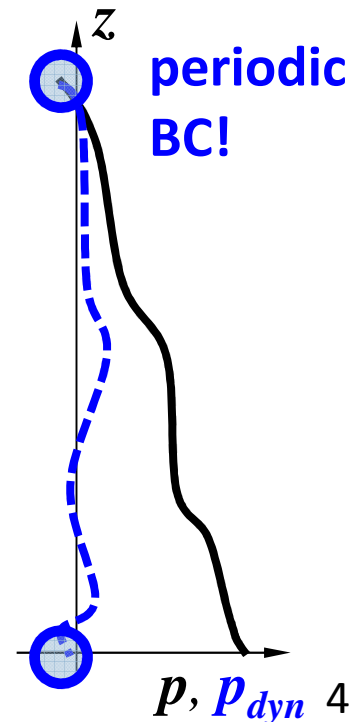
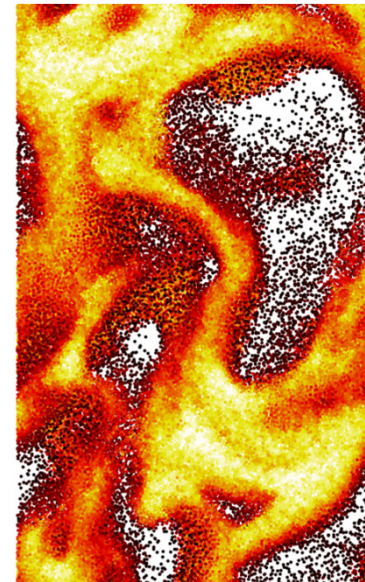
## Momentum Balance Equation in a **Periodic Box**

$$\partial_t (\phi_f \rho_f \mathbf{u}_f) + \nabla \cdot (\phi_f \rho_f \mathbf{u}_f \mathbf{u}_f) = -\phi_f \cdot \nabla p - \nabla \cdot (\phi_f \cdot \boldsymbol{\tau}_f) + \phi_f \rho_f \mathbf{g} + \Phi$$

$$\partial_t (\phi_f \rho_f \mathbf{u}_f) + \nabla \cdot (\phi_f \rho_f \mathbf{u}_f \mathbf{u}_f) = \underbrace{-\phi_f \cdot \nabla p_{dyn}}_{\text{blue box}} - \nabla \cdot (\phi_f \cdot \boldsymbol{\tau}_f) + \underbrace{\phi_f (\rho_f - \rho_{mix}) \mathbf{g}}_{\text{red box}} + \Phi$$

...pressure “as usual”,  
but with different  
meaning!

...treat as explicit term  
in the fluid’s  
momentum balance  
equation



# Drag Model Results (75 $\mu\text{m}$ )

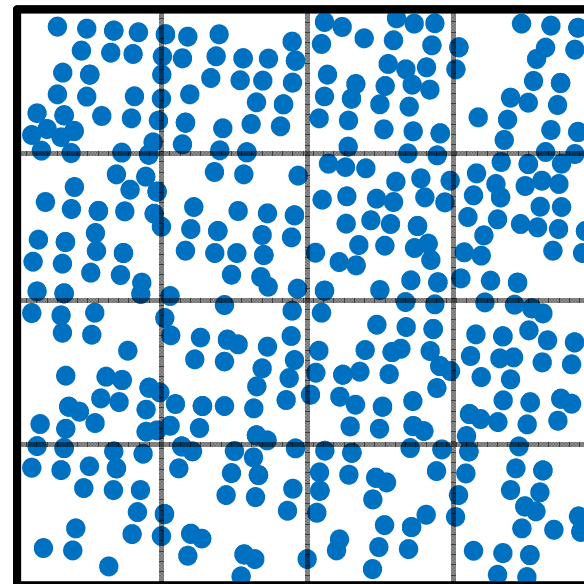
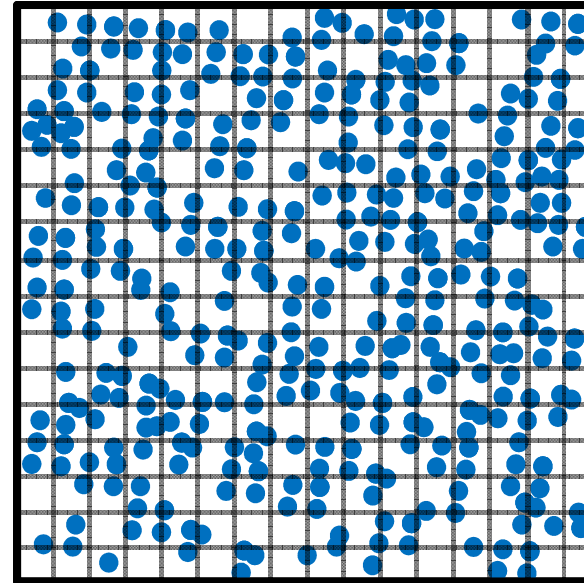
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## 1. CFD-DEM

- Fine fluid grid
- Track all the particles
- Micro-scale drag law
- Obtain filtered drag law

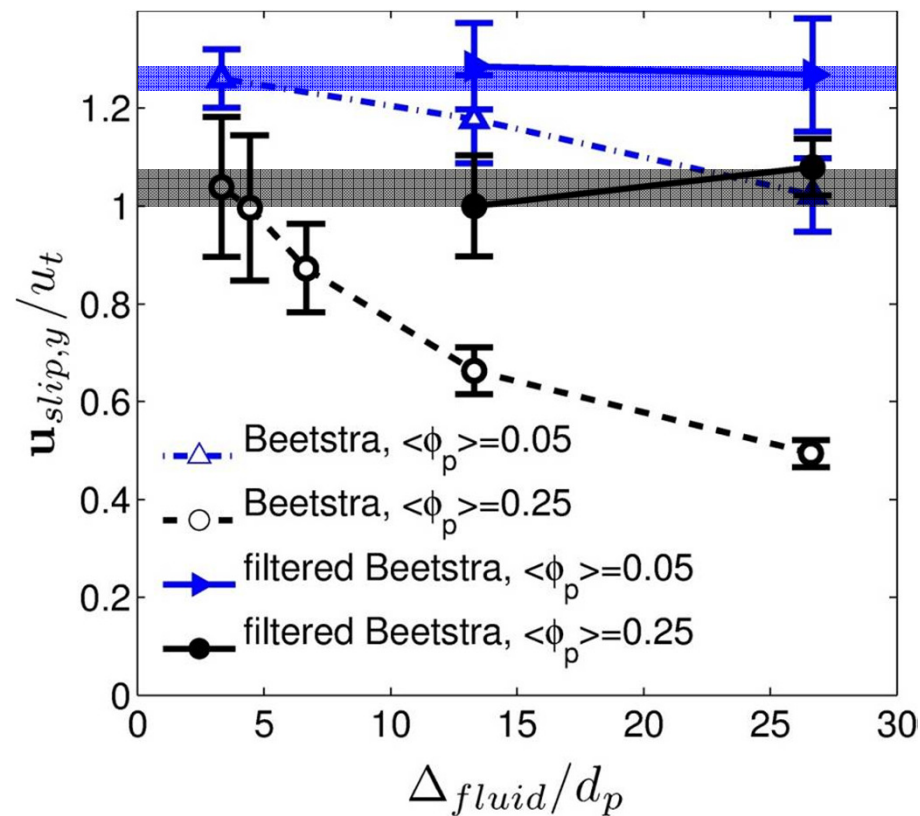
## 2. Coarse Grid CFD-DEM

- Coarse fluid grid
- Track all the particles
- Use filtered drag law



# Drag Model Results (75 $\mu\text{m}$ )

**Q: Do CFD-DEM and Coarse Grid CFD-DEM yield the same results?**



- Large decrease of slip velocity if using “microscopic” drag law (**Beetstra; -53% for  $\langle \phi_p \rangle = 0.25$** ).
- Coarse Grid CFD-DEM with **filtered drag law** is within **+2% ( $\langle \phi_p \rangle = 0.05$ )** and  **$\pm 3.8%$  ( $\langle \phi_p \rangle = 0.25$ )** of well-resolved CFD-DEM!

75  $\mu\text{m}$  particles, 8 x 32 x 8 mm domain, 0.46M - 2.32M particles.

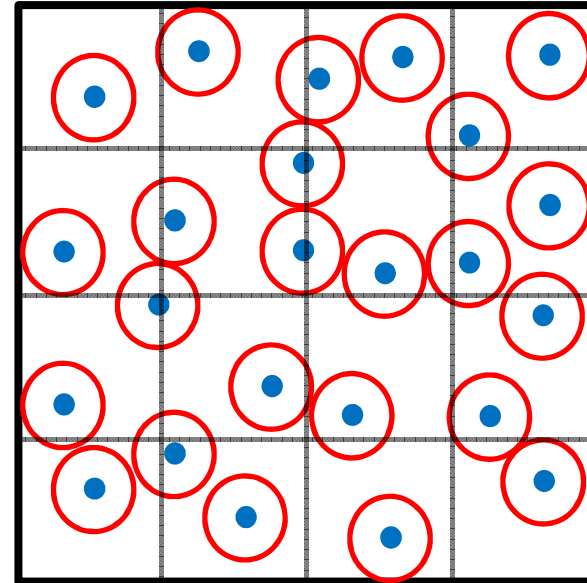
# Drag Model Results (75 $\mu\text{m}$ )

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## 3. CFD-DPM

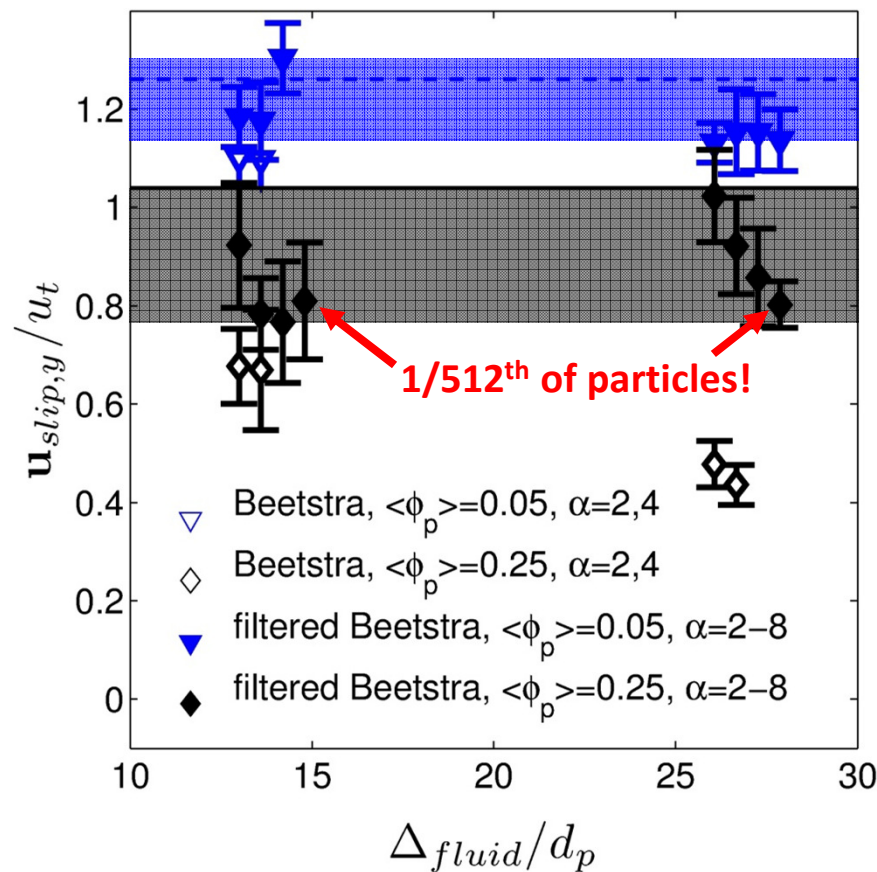
- Use filtered drag law
- Coarse fluid grids
- Track parcels of size

$$d_p = \alpha d_{prim}$$



# Drag Model Results (75 $\mu\text{m}$ )

Q: Do **CFD-DEM** and **CFD-DPM** yield the same results?



- CFD-DPM with “microscopic” drag law significantly under-predicts slip (-58% for  $\langle\phi_p\rangle=0.25$ ).
- **Filtered drag law** improves results, but still significant under prediction: -22% ( $\langle\phi_p\rangle=0.25$ )
- Now, we introduce **a correction to account for parcel size effects**:

$$c_{corr} = \exp[-k(\alpha - 1)]$$

**$k = 0.05$  (based on calibration)**

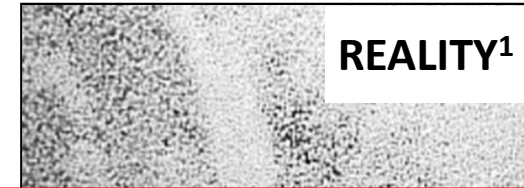
75  $\mu\text{m}$  particles, 8 x 32 x 8 mm domain, 0.46M - 2.32M particles, pairs of symbols represent CFD-DPM result, horizontal lines are results of well-resolved CFD-DEM simulations.



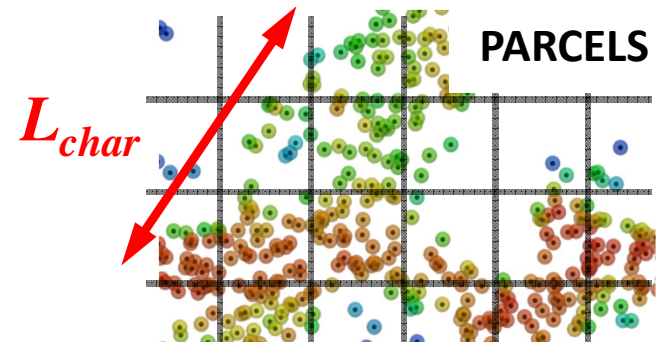
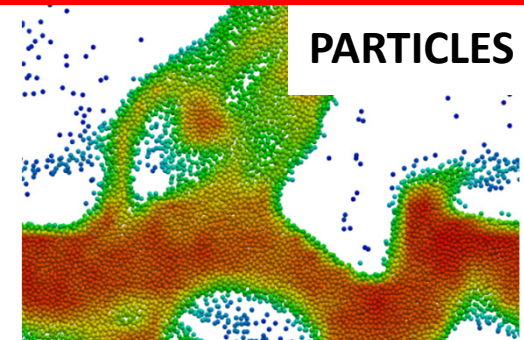
# Outline

- Motivation
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- What is the effective force on an ensemble of particles?
- What is the characteristic size of a particle cluster...  
...to make  $\Delta_{fluid}$  dimensionless?



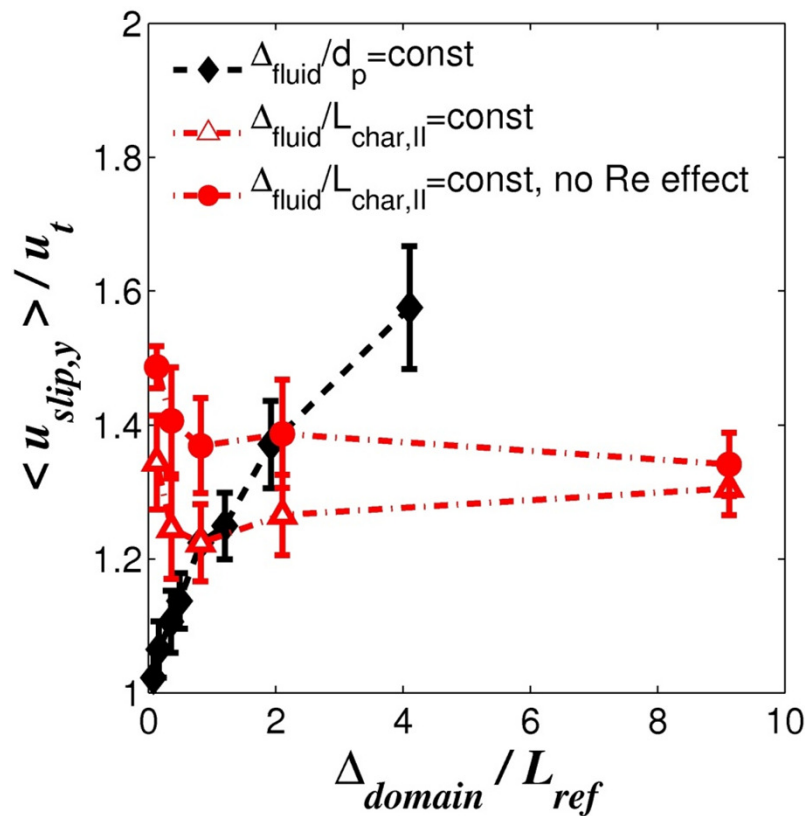
$$\frac{\bar{\beta}_p}{\beta_{p,micro}} = c_{corr}(\alpha) \left[ 1 - f(\Delta_{fluid}, \bar{\phi}_p) h(\bar{\phi}_p) \right]$$



<sup>1</sup>Courtesy: Franklin Shaffer, NETL, Morgantown, WV (2009).

# Drag Model Tests (CFD-DEM)

- Test 1: Use  $d_p$  or  $L_{char,II} = u_t^2 / g Fr_p^{-2/3} = const$  and test sensitivity to  $L_{ref} = u_t^2 / g$

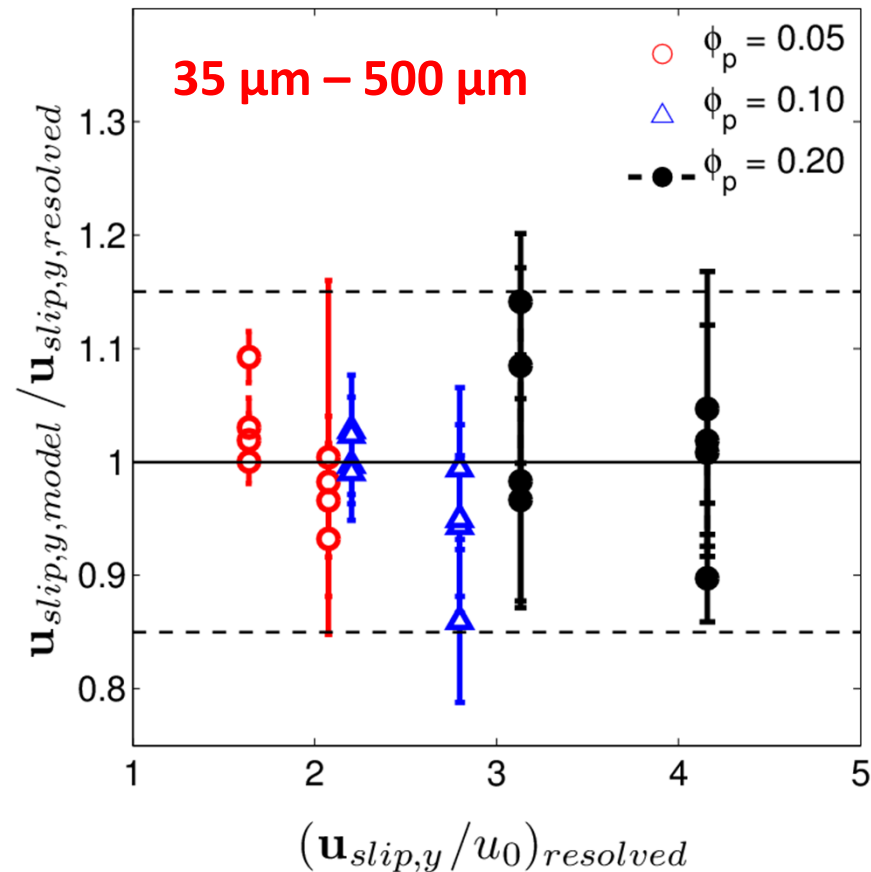
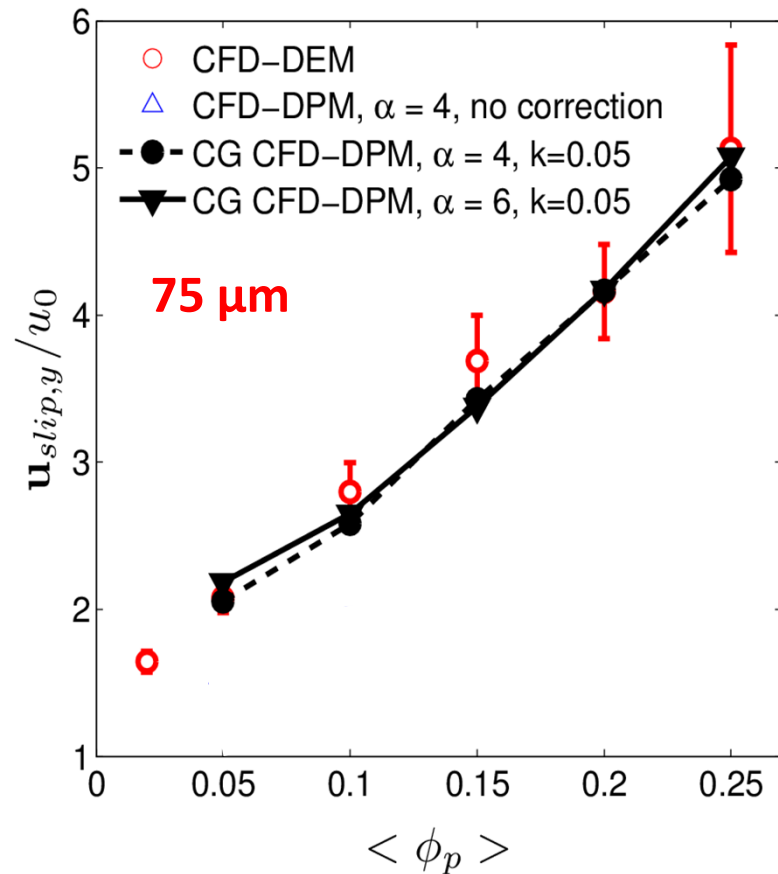


Domain-averaged slip velocity for constant  $L_{char,II}$ , and variation of particle diameter & density ( $\langle \phi_p \rangle = 0.05$ ).

- $\Delta_{fluid} / d_p = const$  **does NOT** yield results independent of  $L_{ref}$ . Same is true for  $\Delta_{fluid} / d_p = const$ .
- $\Delta_{fluid} / L_{char,II} = const$  works much better! This is true with/without Reynolds number dependent drag.
- $L_{char,II}$  **seems to be a useful reference length – WHY?**

# Drag Model Tests

- Test 2: Use  $L_{char,II} = u_t^2 / g Fr_p^{-2/3} = const$  and test sensitivity to  $d_{prim}$  and  $d_p$  for **various**  $\langle \phi_p \rangle$



# Review of Length Scales

## Inspiration from Continuum-Based Theory

- Particle-Phase Momentum Balance\*

$$\rho_p u_t^2 \left[ \frac{1}{u_t} \partial_t (\phi_p \mathbf{u}_p^*) + \nabla \cdot (\phi_p \mathbf{u}_p^* \mathbf{u}_p^*) \right] = -\nabla \cdot \boldsymbol{\sigma}_p - \phi_p \nabla \cdot \boldsymbol{\sigma}_g + \beta u_t \mathbf{u}_{slip}^* + \rho_p \phi_p g \mathbf{g}^*$$

- Estimate** for the **granular temperature** (shear production vs. dissipation)

$$\sqrt{T} \approx \frac{d_p}{L_{visc,II}} u_t$$

- A length scale based on the balance of **viscous particle stress** & **gravity** is:

$$L_{visc,II}^3 \mathbf{g}^* = \left( \frac{u_t^2}{g} \right)^3 \left( \frac{d_p g}{u_t^2} \right)^2 \frac{1}{\phi_p} \cdot \nabla^* \cdot \left[ 2C_{KT} F_{diss}^* (\nabla^* \mathbf{u}_p^* + \nabla \mathbf{u}_p^{*T}) \right] \quad n = -2/3$$

\*with some obvious scalings, however, still no specification of a length scale.

# Summary

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- The advanced drag model takes the effect of **grid resolution, parcels size, local particle concentration and particle properties into account**. It is valid for flow situations **far away from walls**.
- For the smallest **length relevant for particle clustering**, our simulations suggest (tested for  $Re_p = O(1) \dots O(100)$ ):

$$L_{char,II} = \frac{u_t^2}{g} Fr_p^{-2/3}$$

- $L_{char,II}$  appears to be the key **reference length scale for the fluid grid size in coarse-grid simulations**, in case **particle inertia is not that important (compared to  $\rho_p T$ )**.

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